



Designation: D1555 – 16

Standard Test Method for Calculation of Volume and Weight of Industrial Aromatic Hydrocarbons and Cyclohexane¹

This standard is issued under the fixed designation D1555; the number immediately following the designation indicates the year of original adoption or, in the case of revision, the year of last revision. A number in parentheses indicates the year of last reapproval. A superscript epsilon (ϵ) indicates an editorial change since the last revision or reapproval.

This standard has been approved for use by agencies of the U.S. Department of Defense.

1. Scope*

1.1 This standard is for use in calculating the weight and volume of benzene, toluene, mixed xylenes, styrene, ortho-xylene, meta-xylene, para-xylene, cumene, ethylbenzene, 300 to 350°F and 350 to 400°F aromatic hydrocarbons, and cyclohexane. A method is given for calculating the volume at 60°F from an observed volume at $t^\circ\text{F}$. **Table 1** lists the density *in vacuo* at 60°F for chemicals used to develop the relationship. Densities (or weights) “*in vacuo*” represent the true density (or weight) if measured in a vacuum without the buoyancy effect of air acting on the liquid. It is representative of the actual amount of product present. Densities (or weights) “*in air*” represent what would actually be measured on a scale. The difference is on the order of 0.13 %. Modern densitometers measure density *in vacuo* and the ASTM recommends the use of *in vacuo* densities (or weights).

1.2 The values stated in inch-pound units are to be regarded as standard. No other units of measurement are included in this standard.

1.2.1 A complete SI unit companion standard has been developed in Test Method **D1555M**.

1.3 *This standard does not purport to address all of the safety concerns, if any, associated with its use. It is the responsibility of the user of this standard to establish appropriate safety and health practices and determine the applicability of regulatory limitations prior to use.*

2. Referenced Documents

2.1 *ASTM Standards:*²

D1217 Test Method for Density and Relative Density (Spe-

¹ This test method is under the jurisdiction of ASTM Committee **D16** on Aromatic Hydrocarbons and Related Chemicals and is the direct responsibility of Subcommittee **D16.01** on Benzene, Toluene, Xylenes, Cyclohexane and Their Derivatives.

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² For referenced ASTM standards, visit the ASTM website, www.astm.org, or contact ASTM Customer Service at service@astm.org. For *Annual Book of ASTM Standards* volume information, refer to the standard's Document Summary page on the ASTM website.

cific Gravity) of Liquids by Bingham Pycnometer
D1555M Test Method for Calculation of Volume and Weight of Industrial Aromatic Hydrocarbons and Cyclohexane [Metric]

D3505 Test Method for Density or Relative Density of Pure Liquid Chemicals

D4052 Test Method for Density, Relative Density, and API Gravity of Liquids by Digital Density Meter

2.2 *Other Documents:*

American Petroleum Society Research Project 44³

Patterson, J. B., and Morris, E. C. *Metrologia*, 31, 1994, pp. 277-288

NSRDS-NIST 75-121 TRC Thermodynamic Tables—Hydrocarbons, Supplement No. 121, April 30, 2001⁴

3. Significance and Use

3.1 This test method is suitable for use in calculating weights and volumes of the products outlined in Section 1. The information presented in this method can be used for determining quantities of the above-stated aromatic hydrocarbons in tanks, shipping containers, etc.

4. Basic Data

4.1 Densities of materials should be determined by measurement (see Section 7). Densities of pure materials at 60°F may be estimated from densities furnished by NSRDS-NIST 75-121 (National Standard Reference Data Series—National Institute of Standards and Technology).

4.2 The VCF (Volume Correction Factor) equations provided below were derived from the Volume Correction Tables presented in the previous edition of this standard, Method D1555-95. Although reported as based on the American Petroleum Institute Research Project 44, the actual documentation that could be found is incomplete. As regression of the

³ “Selected Values of Properties of Hydrocarbons and Related Compounds,” prepared by American Petroleum Institute Research Project 44 at the Chemical Thermodynamics Center, Department of Chemistry, Texas A&M, College Station, TX.

⁴ Available from National Institute of Standards and Technology (NIST), 100 Bureau Dr., Stop 1070, Gaithersburg, MD 20899-1070, <http://www.nist.gov>.

*A Summary of Changes section appears at the end of this standard

TABLE 1 Physical Properties

| Product | Freezing Point °F | Boiling Point °F | Density <i>in Vacuo</i> at 60°F g/cc ^{A,B} | Density <i>in Vacuo</i> at 60°F lb/gal ^C | Density <i>in Air</i> at 60°F lb/gal ^D |
|------------------|-------------------|------------------|---|---|---|
| Benzene | 42.0 | 176.2 | 0.88373 | 7.3751 | 7.3662 |
| Cumene | -140.9 | 306.3 | 0.86538 | 7.2219 | 7.2130 |
| Cyclohexane | 43.8 | 177.3 | 0.78265 | 6.5315 | 6.5225 |
| Ethylbenzene | -139.0 | 277.1 | 0.87077 | 7.2669 | 7.2580 |
| Styrene | -23.1 | 293.4 | 0.90979 | 7.5926 | 7.5837 |
| Toluene | -139.0 | 231.1 | 0.87096 | 7.2685 | 7.2596 |
| <i>m</i> -Xylene | -54.2 | 282.4 | 0.86784 | 7.2425 | 7.2336 |
| <i>o</i> -Xylene | -13.3 | 291.9 | 0.88340 | 7.3723 | 7.3634 |
| <i>p</i> -Xylene | 55.9 | 281.0 | 0.86456 | 7.2151 | 7.2062 |

^A Based on regression of 2001 TRC Thermodynamic Tables, Hydrocarbons, NSRDS-NIST 75-121 (April 30, 2001). The data is presented in [Appendix X1](#).

^B Specific Gravity has been deleted from this table as unnecessary to this standard. If needed, divide 60°F density in g/cc by 0.999016 g/cc. See [Appendix X2](#).

^C Produced by multiplying the density *in vacuo* at 60°F in g/cc by 8.345404452 and rounding to 4 decimal places.

^D Produced using Density - g/cc *in air* · 1.000149926 – 0.001199407795) · 8.345404452, rounding to 4 decimal places. See [Appendix X3](#).

NIST data ([Appendix X1](#)) provided VCFs that differ from the historical VCFs by only 0 to ± 0.12 % (depending on the compound), a decision was made to use the previous method's VCF tables.

4.3 The VCF tables were regressed with a commercially available data regression program (TableCurve 2D V4). However, any modern regression program should produce the same results.

4.4 The former VCF tables were based on data for compounds used in American Petroleum Institute Research Project 44 for which the purity is not clearly defined, but were reported to be usable for materials in the ranges indicated in [Table 2](#). The data supporting this conclusion appears to be unavailable at the present time; however there is no reason to change this recommendation. If, depending on the composition of the impurities, there is reason to suspect that the VCF implementation procedures presented below do not apply to a particular impure product, a separate implementation procedure should be independently determined. This may be done by measuring the density of a representative sample at different temperatures throughout the expected working temperature range, regressing the data to obtain a temperature/density equation that best reproduces the observed data, and then dividing the constants of the temperature/density equation by the calculated density at 60°F.

TABLE 2 Application Range of Implementation Procedure

| Impure Products | Range |
|---------------------------------|-----------------|
| Benzene | 95 to 100% |
| Cumene | 95 to 100% |
| Cyclohexane | 90 to 100% |
| Ethylbenzene | 95 to 100% |
| Styrene | 95 to 100% |
| Toluene | 95 to 100% |
| Mixed Xylenes | All proportions |
| <i>m</i> -Xylene | 95 to 100% |
| <i>o</i> -Xylene | 95 to 100% |
| <i>p</i> -Xylene | 94 to 100% |
| 300-350°F Aromatic Hydrocarbons | All proportions |
| 350-400°F Aromatic Hydrocarbons | All proportions |

5. Volume Correction Factor Implementation Procedure

5.1 The following general equation is used to generate the Volume Correction Factors:

$$VCF = a + bt + ct^2 + dt^3 + et^4 \quad (1)$$

where:

t = temperature in °F

and constants a through e are specific to each compound (presented in [Table 3](#)).

5.1.1 Temperature may be entered in tenths of a degree Fahrenheit.

5.1.2 The calculated result is rounded to the appropriate significant figures if it is to be reported and not rounded if to be used in another calculation. No intermediate rounding or truncation should be done.

5.1.3 The equations are valid for liquid product up to 140°F (150°F for *p*-xylene).

5.1.4 This implementation procedure replaces the printed table in a previous edition of this standard (Method D1555-95) for determining VCFs. **The implementation procedure is the Standard, not the printed table.** However, the printed table is provided in 1°F increments for the user's convenience ([Table 4](#)).

6. Use of the Implementation Procedure

6.1 *Convert Volume to 60°F*—Enter the appropriate equation with the temperature to the nearest 0.1 degree Fahrenheit at which the bulk volume was measured (temperature t). Multiply the bulk volume measurement at temperature t by the VCF.

6.1.1 *Example 1*—What is the volume at 60°F of a tank car of *p*-xylene whose volume was measured to be 9280 gal at a mean temperature of 88.7°F?

6.1.1.1 Enter 88.7°F and the appropriate constants from [Table 3](#) into [Eq 1](#) to calculate a VCF of 0.984143256178277. Multiply the volume at 88.7°F by the VCF to obtain the volume at 60°F.

$$9280 \text{ gal} \times 0.984143256178277 = 9,132.84941733442 \text{ or } 9133 \text{ gal}$$

If this value is to be reported, it may be rounded as required by the user. The unrounded intermediate value should be used for additional calculations.

TABLE 3 VCF Constants

| Product | a | b | c | d | E |
|-------------------------------|-------------|--------------------------|---------------------------|----------------------------|---------------------------|
| Benzene | 1.038382492 | -6.2307×10^{-4} | -2.8505×10^{-7} | 1.2692×10^{-10} | 0 |
| Cumene | 1.032401114 | -5.3445×10^{-4} | -9.5067×10^{-8} | 3.6272×10^{-11} | 0 |
| Cyclohexane | 1.039337296 | -6.4728×10^{-4} | -1.4582×10^{-7} | 1.03538×10^{-10} | 0 |
| Ethylbenzene | 1.033346632 | -5.5243×10^{-4} | 8.37035×10^{-10} | -1.2692×10^{-9} | 5.55061×10^{-12} |
| Styrene | 1.032227515 | -5.3444×10^{-4} | -4.4323×10^{-8} | 0 | 0 |
| Toluene | 1.035323647 | -5.8887×10^{-4} | 2.46508×10^{-9} | -7.2802×10^{-12} | 0 |
| <i>m</i> -Xylene ^A | 1.031887514 | -5.2326×10^{-4} | -1.3253×10^{-7} | -7.35960×10^{-11} | 0 |
| <i>o</i> -Xylene | 1.031436449 | -5.2302×10^{-4} | -2.5217×10^{-9} | -2.13840×10^{-10} | 0 |
| <i>p</i> -Xylene | 1.032307000 | -5.2815×10^{-4} | -1.8416×10^{-7} | 1.89256×10^{-10} | 0 |
| 300-350°F | 1.031118000 | -5.1827×10^{-4} | -3.5109×10^{-9} | -1.98360×10^{-11} | 0 |
| 350-400°F | 1.029099000 | -4.8287×10^{-4} | -3.7692×10^{-8} | 3.78575×10^{-11} | 0 |

^Aand Mixed Xylenes.

6.2 *Converting Volume to Weight for Chemicals Listed in Table 1*—Convert the measured bulk volume to gallons at 60°F as described in 6.1. Determine the density (all weights *in vacuo*) at 60°F in grams per milliliter (equivalent to grams per cubic centimeter and kilograms per liter) as described in Section 7. To obtain the weight multiply the density in pound per gallon and the volume in gallons. To obtain the density in pounds per gallon *in vacuo* multiple the measured density by 8.345404452. To obtain the pounds per gallon *in air* at 60°F, use the following equation to determine the pound per gallon *in air*, refer to Appendix X3.

$$D_{\text{lb per gallon in air at 60 F}} = [1.000149926 \times D_{\text{in vacuo at 60 F}} - 0.00119940779543] \times 8.345404452$$

To obtain the weight in pounds, multiply the density in pounds per gallon by the volume in gallons.

6.2.1 The density of the *p*-xylene in Example 1 was determined by Test Method D4052 to be 0.8646 g/mL (*in vacuo*) at 60°F. The weight is:

$$9280 \text{ gal} \times 0.984143256178277 \times 8.345404452 \times 0.8646 = 65.897.4967627663 \text{ lb}_{\text{in vacuo}}$$

or

$$9280 \text{ gal} \times 0.984143256178277 \times 8.345404452 \times [1.000149926 \times 0.8646 - 0.0011994077951] = 65,815.960860521 \text{ lb}_{\text{in air}}$$

If this value is to be reported, it may be rounded as required by the user. The unrounded intermediate value should be used for additional calculations.

7. Density Determination

7.1 Density determinations may be carried out by any procedure known to be reliable to at least 4 digits. Test Methods D1217, D3505, and D4052 are suitable and are written to give density *in vacuo*. They should be used with caution, however, as they may be using older data than that upon which this standard is based upon.

8. Precision and Bias

8.1 Since this is a calculation method, no precision and bias statement is required.

9. Keywords

9.1 aromatic; benzene; calculation; conversion; cumene; density; ethylbenzene; *in air*; *in vacuo*; *m*-xylene; mixed xylene; *o*-xylene; *p*-xylene; specific gravity; styrene; 300 to 350°F aromatic hydrocarbons; 350 to 400°F aromatic hydrocarbons; toluene; volume; weight

TABLE 4 Volume Correction Factors

Volume Correction to 60°F

| Temperature °F | Benzene | Cumene | Cyclohexane | Ethylbenzene | Styrene | Toluene | <i>m</i> -Xylene and Mixed Xylenes | <i>o</i> -Xylene | <i>p</i> -Xylene | 300 to 350° Aromatic Hydrocarbons | 350 to 400° Aromatic Hydrocarbons |
|-------------------|---------|---------|-------------|--------------|---------|---------|---|------------------|------------------|---|---|
| -5.0 | ... | ... | ... | ... | ... | 1.03827 | ... | ... | ... | ... | ... |
| -4.0 | ... | ... | ... | ... | ... | 1.03768 | ... | ... | ... | ... | ... |
| -3.0 | ... | ... | ... | ... | ... | 1.03709 | ... | ... | ... | ... | ... |
| -2.0 | ... | ... | ... | ... | ... | 1.03650 | ... | ... | ... | ... | ... |
| -1.0 | ... | ... | ... | ... | ... | 1.03591 | ... | ... | ... | ... | ... |
| 0.0 | ... | ... | ... | ... | ... | 1.03532 | ... | ... | ... | ... | ... |
| 1.0 | ... | ... | ... | ... | ... | 1.03473 | ... | ... | ... | ... | ... |
| 2.0 | ... | ... | ... | ... | ... | 1.03415 | ... | ... | ... | ... | ... |
| 3.0 | ... | ... | ... | ... | ... | 1.03356 | ... | ... | ... | ... | ... |
| 4.0 | ... | ... | ... | ... | ... | 1.03297 | ... | ... | ... | ... | ... |
| 5.0 | ... | 1.02973 | ... | 1.03058 | ... | 1.03238 | 1.02927 | 1.02882 | ... | 1.02853 | 1.02668 |
| 6.0 | ... | 1.02919 | ... | 1.03003 | ... | 1.03179 | 1.02874 | 1.02830 | ... | 1.02801 | 1.02620 |
| 7.0 | ... | 1.02866 | ... | 1.02948 | ... | 1.03120 | 1.02822 | 1.02778 | ... | 1.02749 | 1.02572 |
| 8.0 | ... | 1.02812 | ... | 1.02893 | ... | 1.03061 | 1.02769 | 1.02725 | ... | 1.02697 | 1.02523 |
| 9.0 | ... | 1.02758 | ... | 1.02837 | ... | 1.03002 | 1.02717 | 1.02673 | ... | 1.02645 | 1.02475 |
| 10.0 | ... | 1.02705 | ... | 1.02782 | ... | 1.02944 | 1.02664 | 1.02621 | ... | 1.02593 | 1.02427 |
| 11.0 | ... | 1.02651 | ... | 1.02727 | ... | 1.02885 | 1.02612 | 1.02568 | ... | 1.02542 | 1.02378 |
| 12.0 | ... | 1.02597 | ... | 1.02672 | ... | 1.02826 | 1.02559 | 1.02516 | ... | 1.02490 | 1.02330 |
| 13.0 | ... | 1.02544 | ... | 1.02616 | ... | 1.02767 | 1.02506 | 1.02464 | ... | 1.02438 | 1.02282 |
| 14.0 | ... | 1.02490 | ... | 1.02561 | ... | 1.02708 | 1.02454 | 1.02411 | ... | 1.02386 | 1.02233 |
| 15.0 | ... | 1.02436 | ... | 1.02506 | 1.02420 | 1.02649 | 1.02401 | 1.02359 | ... | 1.02334 | 1.02185 |
| 16.0 | ... | 1.02383 | ... | 1.02450 | 1.02367 | 1.02590 | 1.02348 | 1.02307 | ... | 1.02282 | 1.02136 |
| 17.0 | ... | 1.02329 | ... | 1.02395 | 1.02313 | 1.02531 | 1.02295 | 1.02254 | ... | 1.02231 | 1.02088 |
| 18.0 | ... | 1.02275 | ... | 1.02340 | 1.02259 | 1.02472 | 1.02243 | 1.02202 | ... | 1.02179 | 1.02040 |
| 19.0 | ... | 1.02221 | ... | 1.02284 | 1.02206 | 1.02414 | 1.02190 | 1.02150 | ... | 1.02127 | 1.01991 |
| 20.0 | ... | 1.02167 | ... | 1.02229 | 1.02152 | 1.02355 | 1.02137 | 1.02097 | ... | 1.02075 | 1.01943 |
| 21.0 | ... | 1.02114 | ... | 1.02174 | 1.02098 | 1.02296 | 1.02084 | 1.02045 | ... | 1.02023 | 1.01894 |
| 22.0 | ... | 1.02060 | ... | 1.02118 | 1.02045 | 1.02237 | 1.02031 | 1.01993 | ... | 1.01971 | 1.01846 |
| 23.0 | ... | 1.02006 | ... | 1.02063 | 1.01991 | 1.02178 | 1.01978 | 1.01940 | ... | 1.01920 | 1.01797 |
| 24.0 | ... | 1.01952 | ... | 1.02007 | 1.01938 | 1.02119 | 1.01925 | 1.01888 | ... | 1.01868 | 1.01749 |
| 25.0 | ... | 1.01898 | ... | 1.01952 | 1.01884 | 1.02060 | 1.01872 | 1.01836 | ... | 1.01816 | 1.01700 |
| 26.0 | ... | 1.01844 | ... | 1.01896 | 1.01830 | 1.02001 | 1.01819 | 1.01783 | ... | 1.01764 | 1.01652 |
| 27.0 | ... | 1.01790 | ... | 1.01841 | 1.01777 | 1.01943 | 1.01766 | 1.01731 | ... | 1.01712 | 1.01603 |
| 28.0 | ... | 1.01736 | ... | 1.01785 | 1.01723 | 1.01884 | 1.01713 | 1.01679 | ... | 1.01660 | 1.01555 |
| 29.0 | ... | 1.01682 | ... | 1.01730 | 1.01669 | 1.01825 | 1.01660 | 1.01626 | ... | 1.01608 | 1.01506 |
| 30.0 | ... | 1.01628 | ... | 1.01674 | 1.01615 | 1.01766 | 1.01607 | 1.01574 | ... | 1.01557 | 1.01458 |
| 31.0 | ... | 1.01574 | ... | 1.01619 | 1.01562 | 1.01707 | 1.01554 | 1.01521 | ... | 1.01505 | 1.01409 |
| 32.0 | ... | 1.01520 | ... | 1.01563 | 1.01508 | 1.01648 | 1.01501 | 1.01469 | ... | 1.01453 | 1.01361 |
| 33.0 | ... | 1.01466 | ... | 1.01508 | 1.01454 | 1.01589 | 1.01447 | 1.01417 | ... | 1.01401 | 1.01312 |
| 34.0 | ... | 1.01412 | ... | 1.01452 | 1.01401 | 1.01530 | 1.01394 | 1.01364 | ... | 1.01349 | 1.01264 |
| 35.0 | ... | 1.01358 | ... | 1.01397 | 1.01347 | 1.01472 | 1.01341 | 1.01312 | ... | 1.01297 | 1.01215 |
| 36.0 | ... | 1.01304 | ... | 1.01341 | 1.01293 | 1.01413 | 1.01287 | 1.01259 | ... | 1.01245 | 1.01167 |
| 37.0 | ... | 1.01250 | ... | 1.01285 | 1.01239 | 1.01354 | 1.01234 | 1.01207 | ... | 1.01194 | 1.01118 |
| 38.0 | ... | 1.01196 | ... | 1.01230 | 1.01185 | 1.01295 | 1.01181 | 1.01155 | ... | 1.01142 | 1.01070 |
| 39.0 | ... | 1.01142 | ... | 1.01174 | 1.01132 | 1.01236 | 1.01127 | 1.01102 | ... | 1.01090 | 1.01021 |
| 40.0 | ... | 1.01087 | ... | 1.01118 | 1.01078 | 1.01177 | 1.01074 | 1.01050 | ... | 1.01038 | 1.00973 |
| 41.0 | ... | 1.01033 | ... | 1.01063 | 1.01024 | 1.01118 | 1.01021 | 1.00997 | ... | 1.00986 | 1.00924 |
| 42.0 | ... | 1.00979 | ... | 1.01007 | 1.00970 | 1.01059 | 1.00967 | 1.00945 | ... | 1.00934 | 1.00875 |
| 43.0 | 1.01107 | 1.00925 | ... | 1.00951 | 1.00916 | 1.01001 | 1.00914 | 1.00892 | ... | 1.00882 | 1.00827 |
| 44.0 | 1.01043 | 1.00870 | 1.01058 | 1.00895 | 1.00863 | 1.00942 | 1.00860 | 1.00840 | ... | 1.00831 | 1.00778 |
| 45.0 | 1.00978 | 1.00816 | 1.00992 | 1.00840 | 1.00809 | 1.00883 | 1.00807 | 1.00788 | ... | 1.00779 | 1.00730 |
| 46.0 | 1.00913 | 1.00762 | 1.00926 | 1.00784 | 1.00755 | 1.00824 | 1.00753 | 1.00735 | ... | 1.00727 | 1.00681 |
| 47.0 | 1.00848 | 1.00708 | 1.00860 | 1.00728 | 1.00701 | 1.00765 | 1.00699 | 1.00683 | ... | 1.00675 | 1.00632 |
| 48.0 | 1.00783 | 1.00653 | 1.00794 | 1.00672 | 1.00647 | 1.00706 | 1.00646 | 1.00630 | ... | 1.00623 | 1.00584 |
| 49.0 | 1.00718 | 1.00599 | 1.00728 | 1.00616 | 1.00593 | 1.00647 | 1.00592 | 1.00578 | ... | 1.00571 | 1.00535 |
| 50.0 | 1.00653 | 1.00545 | 1.00662 | 1.00560 | 1.00539 | 1.00589 | 1.00538 | 1.00525 | ... | 1.00519 | 1.00487 |
| 51.0 | 1.00588 | 1.00490 | 1.00596 | 1.00504 | 1.00486 | 1.00530 | 1.00485 | 1.00473 | ... | 1.00467 | 1.00438 |
| 52.0 | 1.00523 | 1.00436 | 1.00530 | 1.00448 | 1.00432 | 1.00471 | 1.00431 | 1.00420 | ... | 1.00416 | 1.00389 |
| 53.0 | 1.00458 | 1.00381 | 1.00464 | 1.00393 | 1.00378 | 1.00412 | 1.00377 | 1.00368 | ... | 1.00364 | 1.00341 |
| 54.0 | 1.00393 | 1.00327 | 1.00398 | 1.00337 | 1.00324 | 1.00353 | 1.00323 | 1.00315 | ... | 1.00312 | 1.00292 |
| 55.0 | 1.00327 | 1.00272 | 1.00331 | 1.00281 | 1.00270 | 1.00294 | 1.00270 | 1.00263 | ... | 1.00260 | 1.00243 |
| 56.0 | 1.00262 | 1.00218 | 1.00265 | 1.00224 | 1.00216 | 1.00235 | 1.00216 | 1.00210 | 1.00219 | 1.00208 | 1.00195 |
| 57.0 | 1.00196 | 1.00164 | 1.00199 | 1.00168 | 1.00162 | 1.00176 | 1.00162 | 1.00158 | 1.00164 | 1.00156 | 1.00146 |
| 58.0 | 1.00131 | 1.00109 | 1.00132 | 1.00112 | 1.00108 | 1.00118 | 1.00108 | 1.00105 | 1.00109 | 1.00104 | 1.00097 |
| 59.0 | 1.00066 | 1.00055 | 1.00066 | 1.00056 | 1.00054 | 1.00059 | 1.00054 | 1.00053 | 1.00054 | 1.00052 | 1.00049 |
| 60.0 | 1.00000 | 1.00000 | 1.00000 | 1.00000 | 1.00000 | 1.00000 | 1.00000 | 1.00000 | 1.00000 | 1.00000 | 1.00000 |
| 61.0 | 0.99934 | 0.99945 | 0.99933 | 0.99944 | 0.99946 | 0.99941 | 0.99946 | 0.99947 | 0.99945 | 0.99949 | 0.99951 |
| 62.0 | 0.99869 | 0.99891 | 0.99867 | 0.99888 | 0.99892 | 0.99882 | 0.99892 | 0.99895 | 0.99890 | 0.99897 | 0.99903 |
| 63.0 | 0.99803 | 0.99836 | 0.99801 | 0.99832 | 0.99838 | 0.99823 | 0.99838 | 0.99842 | 0.99835 | 0.99845 | 0.99854 |
| 64.0 | 0.99737 | 0.99782 | 0.99734 | 0.99775 | 0.99784 | 0.99764 | 0.99784 | 0.99790 | 0.99780 | 0.99793 | 0.99805 |
| 65.0 | 0.99671 | 0.99727 | 0.99668 | 0.99719 | 0.99730 | 0.99706 | 0.99730 | 0.99737 | 0.99725 | 0.99741 | 0.99756 |

TABLE 4 *Continued*

Volume Correction to 60°F

| Temperature °F | Benzene | Cumene | Cyclohexane | Ethylbenzene | Styrene | Toluene | <i>m</i> -Xylene and Mixed Xylenes | <i>o</i> -Xylene | <i>p</i> -Xylene | 300 to 350° Aromatic Hydrocarbons | 350 to 400° Aromatic Hydrocarbons |
|-------------------|---------|---------|-------------|--------------|---------|---------|---|------------------|------------------|---|---|
| 66.0 | 0.99605 | 0.99672 | 0.99601 | 0.99663 | 0.99676 | 0.99647 | 0.99675 | 0.99684 | 0.99670 | 0.99689 | 0.99708 |
| 67.0 | 0.99540 | 0.99618 | 0.99535 | 0.99607 | 0.99622 | 0.99588 | 0.99621 | 0.99632 | 0.99615 | 0.99637 | 0.99659 |
| 68.0 | 0.99474 | 0.99563 | 0.99468 | 0.99550 | 0.99568 | 0.99529 | 0.99567 | 0.99579 | 0.99560 | 0.99585 | 0.99610 |
| 69.0 | 0.99408 | 0.99508 | 0.99401 | 0.99494 | 0.99514 | 0.99470 | 0.99513 | 0.99527 | 0.99505 | 0.99533 | 0.99561 |
| 70.0 | 0.99341 | 0.99454 | 0.99335 | 0.99438 | 0.99460 | 0.99411 | 0.99458 | 0.99474 | 0.99450 | 0.99482 | 0.99513 |
| 71.0 | 0.99275 | 0.99399 | 0.99268 | 0.99382 | 0.99406 | 0.99352 | 0.99404 | 0.99421 | 0.99395 | 0.99430 | 0.99464 |
| 72.0 | 0.99209 | 0.99344 | 0.99202 | 0.99325 | 0.99352 | 0.99294 | 0.99350 | 0.99369 | 0.99340 | 0.99378 | 0.99415 |
| 73.0 | 0.99143 | 0.99289 | 0.99135 | 0.99269 | 0.99298 | 0.99235 | 0.99295 | 0.99316 | 0.99284 | 0.99326 | 0.99366 |
| 74.0 | 0.99077 | 0.99235 | 0.99068 | 0.99212 | 0.99244 | 0.99176 | 0.99241 | 0.99263 | 0.99229 | 0.99274 | 0.99318 |
| 75.0 | 0.99010 | 0.99180 | 0.99001 | 0.99156 | 0.99190 | 0.99117 | 0.99187 | 0.99211 | 0.99174 | 0.99222 | 0.99269 |
| 76.0 | 0.98944 | 0.99125 | 0.98935 | 0.99099 | 0.99135 | 0.99058 | 0.99132 | 0.99158 | 0.99119 | 0.99170 | 0.99220 |
| 77.0 | 0.98877 | 0.99070 | 0.98868 | 0.99043 | 0.99081 | 0.98999 | 0.99078 | 0.99105 | 0.99063 | 0.99118 | 0.99171 |
| 78.0 | 0.98811 | 0.99015 | 0.98801 | 0.98987 | 0.99027 | 0.98940 | 0.99023 | 0.99052 | 0.99008 | 0.99066 | 0.99122 |
| 79.0 | 0.98744 | 0.98960 | 0.98734 | 0.98930 | 0.98973 | 0.98881 | 0.98969 | 0.99000 | 0.98953 | 0.99014 | 0.99074 |
| 80.0 | 0.98678 | 0.98906 | 0.98667 | 0.98874 | 0.98919 | 0.98823 | 0.98914 | 0.98947 | 0.98897 | 0.98962 | 0.99025 |
| 81.0 | 0.98611 | 0.98851 | 0.98601 | 0.98817 | 0.98865 | 0.98764 | 0.98859 | 0.98894 | 0.98842 | 0.98910 | 0.98976 |
| 82.0 | 0.98544 | 0.98796 | 0.98534 | 0.98760 | 0.98811 | 0.98705 | 0.98805 | 0.98841 | 0.98786 | 0.98859 | 0.98927 |
| 83.0 | 0.98478 | 0.98741 | 0.98467 | 0.98704 | 0.98756 | 0.98646 | 0.98750 | 0.98789 | 0.98731 | 0.98807 | 0.98878 |
| 84.0 | 0.98411 | 0.98686 | 0.98400 | 0.98647 | 0.98702 | 0.98587 | 0.98695 | 0.98736 | 0.98676 | 0.98755 | 0.98829 |
| 85.0 | 0.98344 | 0.98631 | 0.98333 | 0.98591 | 0.98648 | 0.98528 | 0.98641 | 0.98683 | 0.98620 | 0.98703 | 0.98781 |
| 86.0 | 0.98277 | 0.98576 | 0.98266 | 0.98534 | 0.98594 | 0.98469 | 0.98586 | 0.98630 | 0.98564 | 0.98651 | 0.98732 |
| 87.0 | 0.98210 | 0.98521 | 0.98199 | 0.98477 | 0.98540 | 0.98411 | 0.98531 | 0.98577 | 0.98509 | 0.98599 | 0.98683 |
| 88.0 | 0.98143 | 0.98466 | 0.98132 | 0.98421 | 0.98485 | 0.98352 | 0.98476 | 0.98525 | 0.98453 | 0.98547 | 0.98634 |
| 89.0 | 0.98076 | 0.98411 | 0.98065 | 0.98364 | 0.98431 | 0.98293 | 0.98422 | 0.98472 | 0.98398 | 0.98495 | 0.98585 |
| 90.0 | 0.98009 | 0.98356 | 0.97998 | 0.98307 | 0.98377 | 0.98234 | 0.98367 | 0.98419 | 0.98342 | 0.98443 | 0.98536 |
| 91.0 | 0.97942 | 0.98301 | 0.97931 | 0.98251 | 0.98323 | 0.98175 | 0.98312 | 0.98366 | 0.98286 | 0.98391 | 0.98487 |
| 92.0 | 0.97875 | 0.98246 | 0.97863 | 0.98194 | 0.98268 | 0.98116 | 0.98257 | 0.98313 | 0.98231 | 0.98339 | 0.98439 |
| 93.0 | 0.97807 | 0.98190 | 0.97796 | 0.98137 | 0.98214 | 0.98057 | 0.98202 | 0.98260 | 0.98175 | 0.98287 | 0.98390 |
| 94.0 | 0.97740 | 0.98135 | 0.97729 | 0.98080 | 0.98160 | 0.97999 | 0.98147 | 0.98207 | 0.98119 | 0.98235 | 0.98341 |
| 95.0 | 0.97673 | 0.98080 | 0.97662 | 0.98024 | 0.98106 | 0.97940 | 0.98092 | 0.98154 | 0.98063 | 0.98183 | 0.98292 |
| 96.0 | 0.97605 | 0.98025 | 0.97595 | 0.97967 | 0.98051 | 0.97881 | 0.98037 | 0.98101 | 0.98007 | 0.98131 | 0.98243 |
| 97.0 | 0.97538 | 0.97970 | 0.97527 | 0.97910 | 0.97997 | 0.97822 | 0.97982 | 0.98048 | 0.97952 | 0.98079 | 0.98194 |
| 98.0 | 0.97470 | 0.97915 | 0.97460 | 0.97853 | 0.97943 | 0.97763 | 0.97927 | 0.97996 | 0.97896 | 0.98028 | 0.98145 |
| 99.0 | 0.97403 | 0.97859 | 0.97393 | 0.97797 | 0.97888 | 0.97704 | 0.97871 | 0.97943 | 0.97840 | 0.97976 | 0.98096 |
| 100.0 | 0.97335 | 0.97804 | 0.97325 | 0.97740 | 0.97834 | 0.97645 | 0.97816 | 0.97890 | 0.97784 | 0.97924 | 0.98047 |
| 101.0 | 0.97268 | 0.97749 | 0.97258 | 0.97683 | 0.97780 | 0.97587 | 0.97761 | 0.97837 | 0.97728 | 0.97872 | 0.97998 |
| 102.0 | 0.97200 | 0.97694 | 0.97191 | 0.97626 | 0.97725 | 0.97528 | 0.97706 | 0.97784 | 0.97672 | 0.97820 | 0.97949 |
| 103.0 | 0.97132 | 0.97638 | 0.97123 | 0.97569 | 0.97671 | 0.97469 | 0.97651 | 0.97730 | 0.97616 | 0.97768 | 0.97900 |
| 104.0 | 0.97064 | 0.97583 | 0.97056 | 0.97512 | 0.97617 | 0.97410 | 0.97595 | 0.97677 | 0.97560 | 0.97716 | 0.97852 |
| 105.0 | 0.96996 | 0.97528 | 0.96989 | 0.97456 | 0.97562 | 0.97351 | 0.97540 | 0.97624 | 0.97504 | 0.97664 | 0.97803 |
| 106.0 | 0.96929 | 0.97472 | 0.96921 | 0.97399 | 0.97508 | 0.97292 | 0.97485 | 0.97571 | 0.97448 | 0.97612 | 0.97754 |
| 107.0 | 0.96861 | 0.97417 | 0.96854 | 0.97342 | 0.97453 | 0.97233 | 0.97429 | 0.97518 | 0.97392 | 0.97560 | 0.97705 |
| 108.0 | 0.96793 | 0.97362 | 0.96786 | 0.97285 | 0.97399 | 0.97175 | 0.97374 | 0.97465 | 0.97336 | 0.97508 | 0.97656 |
| 109.0 | 0.96725 | 0.97306 | 0.96719 | 0.97228 | 0.97345 | 0.97116 | 0.97318 | 0.97412 | 0.97280 | 0.97456 | 0.97607 |
| 110.0 | 0.96656 | 0.97251 | 0.96651 | 0.97171 | 0.97290 | 0.97057 | 0.97263 | 0.97359 | 0.97223 | 0.97404 | 0.97558 |
| 111.0 | 0.96588 | 0.97196 | 0.96583 | 0.97114 | 0.97236 | 0.96998 | 0.97207 | 0.97306 | 0.97167 | 0.97352 | 0.97509 |
| 112.0 | 0.96520 | 0.97140 | 0.96516 | 0.97058 | 0.97181 | 0.96939 | 0.97152 | 0.97253 | 0.97111 | 0.97300 | 0.97460 |
| 113.0 | 0.96452 | 0.97085 | 0.96448 | 0.97001 | 0.97127 | 0.96880 | 0.97096 | 0.97199 | 0.97055 | 0.97248 | 0.97411 |
| 114.0 | 0.96384 | 0.97029 | 0.96381 | 0.96944 | 0.97073 | 0.96821 | 0.97040 | 0.97146 | 0.96998 | 0.97196 | 0.97362 |
| 115.0 | 0.96315 | 0.96974 | 0.96313 | 0.96887 | 0.97018 | 0.96763 | 0.96985 | 0.97093 | 0.96942 | 0.97144 | 0.97313 |
| 116.0 | 0.96247 | 0.96918 | 0.96245 | 0.96830 | 0.96964 | 0.96704 | 0.96929 | 0.97040 | 0.96886 | 0.97092 | 0.97264 |
| 117.0 | 0.96178 | 0.96863 | 0.96178 | 0.96773 | 0.96909 | 0.96645 | 0.96873 | 0.96987 | 0.96830 | 0.97040 | 0.97215 |
| 118.0 | 0.96110 | 0.96807 | 0.96110 | 0.96716 | 0.96855 | 0.96586 | 0.96818 | 0.96933 | 0.96773 | 0.96988 | 0.97166 |
| 119.0 | 0.96041 | 0.96752 | 0.96042 | 0.96659 | 0.96800 | 0.96527 | 0.96762 | 0.96880 | 0.96717 | 0.96936 | 0.97117 |
| 120.0 | 0.95973 | 0.96696 | 0.95974 | 0.96602 | 0.96746 | 0.96468 | 0.96706 | 0.96827 | 0.96660 | 0.96884 | 0.97068 |
| 121.0 | 0.95904 | 0.96641 | 0.95906 | 0.96546 | 0.96691 | 0.96409 | 0.96650 | 0.96774 | 0.96604 | 0.96832 | 0.97019 |
| 122.0 | 0.95836 | 0.96585 | 0.95839 | 0.96489 | 0.96637 | 0.96350 | 0.96594 | 0.96720 | 0.96548 | 0.96780 | 0.96970 |
| 123.0 | 0.95767 | 0.96529 | 0.95771 | 0.96432 | 0.96582 | 0.96292 | 0.96538 | 0.96667 | 0.96491 | 0.96728 | 0.96921 |
| 124.0 | 0.95698 | 0.96474 | 0.95703 | 0.96375 | 0.96528 | 0.96233 | 0.96483 | 0.96614 | 0.96435 | 0.96676 | 0.96872 |
| 125.0 | 0.95629 | 0.96418 | 0.95635 | 0.96318 | 0.96473 | 0.96174 | 0.96427 | 0.96560 | 0.96378 | 0.96624 | 0.96823 |
| 126.0 | 0.95560 | 0.96362 | 0.95567 | 0.96261 | 0.96418 | 0.96115 | 0.96371 | 0.96507 | 0.96321 | 0.96572 | 0.96773 |
| 127.0 | 0.95492 | 0.96307 | 0.95499 | 0.96205 | 0.96364 | 0.96056 | 0.96315 | 0.96453 | 0.96265 | 0.96520 | 0.96724 |
| 128.0 | 0.95423 | 0.96251 | 0.95431 | 0.96148 | 0.96309 | 0.95997 | 0.96258 | 0.96400 | 0.96208 | 0.96468 | 0.96675 |
| 129.0 | 0.95354 | 0.96195 | 0.95363 | 0.96091 | 0.96255 | 0.95938 | 0.96202 | 0.96347 | 0.96152 | 0.96416 | 0.96626 |
| 130.0 | 0.95284 | 0.96140 | 0.95295 | 0.96034 | 0.96200 | 0.95880 | 0.96146 | 0.96293 | 0.96095 | 0.96364 | 0.96577 |
| 131.0 | 0.95215 | 0.96084 | 0.95227 | 0.95977 | 0.96146 | 0.95821 | 0.96090 | 0.96240 | 0.96038 | 0.96312 | 0.96528 |
| 132.0 | 0.95146 | 0.96028 | 0.95159 | 0.95921 | 0.96091 | 0.95762 | 0.96034 | 0.96186 | 0.95982 | 0.96260 | 0.96479 |
| 133.0 | 0.95077 | 0.95972 | 0.95091 | 0.95864 | 0.96036 | 0.95703 | 0.95978 | 0.96133 | 0.95925 | 0.96208 | 0.96430 |
| 134.0 | 0.95008 | 0.95917 | 0.95023 | 0.95807 | 0.95982 | 0.95644 | 0.95921 | 0.96079 | 0.95868 | 0.96156 | 0.96381 |
| 135.0 | 0.94939 | 0.95861 | 0.94955 | 0.95750 | 0.95927 | 0.95585 | 0.95865 | 0.96026 | 0.95812 | 0.96104 | 0.96332 |
| 136.0 | 0.94869 | 0.95805 | 0.94887 | 0.95694 | 0.95872 | 0.95526 | 0.95809 | 0.95972 | 0.95755 | 0.96052 | 0.96283 |

TABLE 4 *Continued*

Volume Correction to 60°F

| Temperature °F | Benzene | Cumene | Cyclohexane | Ethylbenzene | Styrene | Toluene | <i>m</i> -Xylene and Mixed Xylenes | <i>o</i> -Xylene | <i>p</i> -Xylene | 300 to 350° Aromatic Hydrocarbons | 350 to 400° Aromatic Hydrocarbons |
|-------------------|---------|---------|-------------|--------------|---------|---------|---|------------------|------------------|---|---|
| 137.0 | 0.94800 | 0.95749 | 0.94819 | 0.95637 | 0.95818 | 0.95468 | 0.95752 | 0.95919 | 0.98698 | 0.96000 | 0.96234 |
| 138.0 | 0.94730 | 0.95693 | 0.94751 | 0.95580 | 0.95763 | 0.95409 | 0.95696 | 0.95865 | 0.95641 | 0.95948 | 0.96184 |
| 139.0 | 0.94661 | 0.95637 | 0.94683 | 0.95524 | 0.95708 | 0.95350 | 0.95640 | 0.95811 | 0.95584 | 0.95896 | 0.96135 |
| 140.0 | 0.94591 | 0.95581 | 0.94614 | 0.95467 | 0.95654 | 0.95291 | 0.95583 | 0.95758 | 0.95528 | 0.95844 | 0.96086 |
| 141.0 | ... | ... | ... | ... | ... | ... | ... | ... | 0.95471 | ... | ... |
| 142.0 | ... | ... | ... | ... | ... | ... | ... | ... | 0.95414 | ... | ... |
| 143.0 | ... | ... | ... | ... | ... | ... | ... | ... | 0.95357 | ... | ... |
| 144.0 | ... | ... | ... | ... | ... | ... | ... | ... | 0.95300 | ... | ... |
| 145.0 | ... | ... | ... | ... | ... | ... | ... | ... | 0.95243 | ... | ... |
| 146.0 | ... | ... | ... | ... | ... | ... | ... | ... | 0.95186 | ... | ... |
| 147.0 | ... | ... | ... | ... | ... | ... | ... | ... | 0.95129 | ... | ... |
| 148.0 | ... | ... | ... | ... | ... | ... | ... | ... | 0.95072 | ... | ... |
| 149.0 | ... | ... | ... | ... | ... | ... | ... | ... | 0.95015 | ... | ... |
| 150.0 | ... | ... | ... | ... | ... | ... | ... | ... | 0.94958 | ... | ... |

APPENDIXES

(Nonmandatory Information)

X1. DENSITY DATA EXTRACTED FROM NSRDS-NIST 75-121 (TRC THERMODYNAMIC TABLES, HYDROCARBONS)

This Appendix is included for documentation purposes only and is not necessary for implementation of this standard.

| °C | benzene kg/m ³ | cumene kg/m ³ | cyclohexane kg/m ³ | ethylbenzene kg/m ³ | styrene kg/m ³ | toluene kg/m ³ | <i>m</i> -xylene kg/m ³ | <i>o</i> -xylene kg/m ³ | <i>p</i> -xylene kg/m ³ |
|-----|------------------------------|-----------------------------|----------------------------------|-----------------------------------|------------------------------|------------------------------|---------------------------------------|---------------------------------------|---------------------------------------|
| -30 | ... | A | ... | A | A | A | A | ... | ... |
| -20 | ... | 894.8 | ... | 901.1 | 942.5 | 903.6 | 897.3 | 912.0 | ... |
| -10 | ... | 886.6 | ... | 892.7 | 933.3 | 894.5 | 889.1 | 904.1 | ... |
| 0 | ... | 878.4 | 797.0 | 884.2 | 924.1 | 885.3 | 880.8 | 896.0 | ... |
| 10 | 889.66 | 870.0 | 787.79 | 875.57 | 914.9 | 876.10 | 872.50 | 887.93 | ... |
| 15 | ... | ... | ... | ... | 910.3 | ... | ... | ... | ... |
| 20 | 879.00 | 861.7 | 778.53 | 866.92 | 905.7 | 866.84 | 864.10 | 879.75 | 860.91 |
| 25 | 873.66 | ... | 773.87 | 862.57 | 901.1 | ... | 859.86 | ... | ... |
| 30 | 868.30 | 853.2 | 769.18 | 858.2 | 896.5 | 857.53 | 855.61 | 871.49 | 852.32 |
| 40 | 857.5 | 844.7 | 759.71 | 849.4 | 887.3 | 848.2 | 847.0 | 863.2 | 843.6 |
| 50 | 846.7 | 836.1 | 750.11 | 840.5 | 878.1 | 838.7 | 838.4 | 854.7 | 834.9 |
| 60 | 835.8 | 827.5 | 740.4 | 831.6 | 868.9 | 829.2 | 829.6 | 846.2 | 826.0 |
| 70 | A | A | A | A | A | A | A | A | 817.1 |
| 80 | ... | ... | ... | ... | ... | ... | ... | ... | A |

^A Data extends beyond that shown.

X2. PHYSICAL CONSTANTS

This Appendix is included for documentation purposes only and is not necessary for implementation of this standard.

X2.1 *Constants and Factors Used in Calculations*—(NIST Handbook 44, Appendix C: <http://www.nist.gov/pml/wmd/pubs/hb44.cfm>)

$$\begin{aligned} 1 \text{ lb} &= 453.59237 \text{ g} \\ 1 \text{ U.S. gal} &= 231 \text{ in}^3 \\ 1 \text{ in}^3 &= 16.387064 \text{ mL} \end{aligned}$$

X2.2 *Density of Weights*—NIST Handbook 44 Appendix B and Handbook 105–1 state that brass is no longer used for balance weights due to its softness. A generic reference weight density of 8.0 g/cm³ at 20°C is used by international agreement. Since a specific material is no longer specified, no calculation of density at reference temperature can be made.

$$B^{68} = 8.0 \text{ g/cm}^3$$

X2.3 *Density of Standard Air*—NIST Handbook 44 Appendix B and Handbook 105–1 specify a temperature of 20°C for air buoyancy calculations. The latest International Committee of Weights and Measures (CIPM) 81/91 Air Density Executable File yields a density of 0.001199228 g/cm³ (760 mm, 50 % humidity, 20°C).

X2.4 *Density of Water*—The equation of J. B. Patterson and E. C. Morris yields a density of water at 60°F of 0.999016 g/mL.

X3. DENSITY AT 60°F IN AIR EQUIVALENT TO ABSOLUTE DENSITY AT 60°F

This Appendix is included for documentation purposes only and is not necessary for implementation of this standard.

X3.1 The following is a derivation of the equation for converting density *in vacuo* to density *in air*.

X3.1.1 Consider mass *d* to be measured balanced on a scale *in vacuo* (no air) by an equal reference mass *b*. When balanced, all forces acting on the system cancel each other. Thus, force $F_d = m_d \cdot a$ (*a* = acceleration of gravity) acting on the mass m_d is balanced by an equal force $F_b = m_b \cdot a$ on the reference mass m_b .

$$\begin{aligned} F_d &= F_b \\ m_d \cdot a &= m_b \cdot a \end{aligned}$$

X3.1.2 When balanced *in air*, each mass is counteracted by a force equal to the weight of the air it displaces (Archimedes's principle). Therefore, $F_{ad} = m_{ad} \cdot a$ and $F_{ab} = m_{ab} \cdot a$, where m_{ad} is the mass of air displacing m_d and m_{ab} is the mass of air displacing m_b .

$$\begin{aligned} F_d - F_{ad} &= F_b - F_{ab} \\ m_d \cdot a - m_{ad} \cdot a &= m_b \cdot a - m_{ab} \cdot a \\ m_d - m_{ad} &= m_b - m_{ab} \end{aligned}$$

X3.1.3 Multiplying the right side of the equation by one in the form of m_b/m_b gives:

$$m_d - m_{ad} = \frac{m_b - m_{ab}}{m_b} \cdot m_b$$

X3.1.4 Similarly, multiplying each side of the equation by the volumes involved (V_d for mass m_d , V_b for mass m_b):

$$\begin{aligned} (m_d - m_{ad}) \cdot \frac{V_d}{V_d} &= \frac{1/V_b}{1/V_b} \cdot \frac{(m_b - m_{ab})}{m_b} \cdot m_b \\ \left(\frac{m_d}{V_d} - \frac{m_{ad}}{V_d} \right) &= \frac{m_b/V_b - m_{ab}/V_b}{m_b/V_b} \cdot [m_b/V_d] \end{aligned}$$

X3.1.5 For volumes at 60°F, these ratios are densities at 60°F. However, the air and reference weight densities to be

used for air buoyancy corrections are at 20°C (68°F) by international agreement ([Appendix X2](#)); the difference between the ratio of the densities at 20°C (68°F) and that at 60°F is considered negligible. Thus:

$$\begin{aligned} D^{60} - A^{68} &= \frac{B^{68} - A^{68}}{B^{68}} \cdot [m_b/V_d]^{60} \\ [m_b/V_d]^{60} &= \frac{D^{60} - A^{68}}{B^{68} - A^{68}} = \frac{D^{60} - A^{68}}{1 - (A^{68}/B^{68})} \end{aligned}$$

where:

D^{60} = density of liquid at 60°F *in vacuo*, m_d / V_d
 A^{68} = density of standard air at 68°F *in vacuo*, m_{ad} / V_d or m_{ab} / V_b ,
 B^{68} = density of reference weights at 68°F *in vacuo*, m_b / V_b , and
 $[m_b/V_d]^{60}$ = density of liquid at 60°F *in air* (when balanced, the mass of the reference equals the mass of the liquid).

X3.1.6 Selection of the proper conversion factor *f* is used to change units from one unit system to another, say, g/mL to lb/gal (or any other expression of density).

$$[m_b/V_d]^{60} = \frac{D^{60} - A^{68}}{1 - (A^{68}/B^{68})} \cdot f$$

X3.1.7 Substituting with the values from [Appendix X2](#), this equation becomes:

$$[m_b/V_d]^{60} = [1.000149926 \cdot D^{60} - 0.001199407795] \cdot f$$

$$f = \frac{1 \text{ lb}}{453.59237 \text{ g}} \times \frac{231 \text{ in}^3}{\text{gallon}} \times \frac{16.387064 \text{ mL}}{\text{in}^3}$$

$$f = 8.345404452 \frac{\text{lb} \times \text{mL}}{\text{gal} \times \text{g}}$$

SUMMARY OF CHANGES

Committee D16 has identified the location of selected changes to this standard since the last issue (D1555 - 09) that may impact the use of this standard. (Approved November 1, 2016.)

- | | |
|---|---|
| (1) Some editorial remarks have been removed from the method. | (3) The use of Table 1 for determining base density was eliminated. |
| (2) The method of arithmetically averaging the pure densities for a mixture was eliminated. | (4) The rounding of the results has been explicitly defined. |

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